

Environmental Fluid Dynamics: Lecture 14

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- 1 Atmospheric Dynamics: Basic Equations
 - Summation Review
 - Mechanical Energy Equation
 - Thermal Energy Equation

- 2 Summary



Summation Review

Einstein Summation Review

Consider:

$U_m \Rightarrow$ generic velocity vector

$x_m \Rightarrow$ generic component of distance

$e_m \Rightarrow$ generic unit vector

where $m = 1, 2, 3$. We can write the individual components as:

$$\begin{array}{lll} U_1 = u & x_1 = x & e_1 = \hat{i} \\ U_2 = v & x_2 = x & e_2 = \hat{j} \\ U_3 = w & x_3 = x & e_3 = \hat{k} \end{array}$$

A variable with:

- no free indices is a **scalar**.
- one free indice is a **vector**.
- two free indices is a **tensor**.



There are two primary summation operators that we will use:

- **Kronecker Delta**

$$\delta_{mn} = \begin{cases} +1, & \text{if } m = n \\ 0 & \text{if } m \neq n \end{cases}$$

- **Levi-Civita (Alternating Unit) Tensor**

$$\epsilon_{mnq} = \begin{cases} +1, & \text{if } mnq = 123, 231, 312 & \text{even permutation} \\ -1 & \text{if } mnq = 321, 213, 132 & \text{odd permutation} \\ 0 & \text{if } m = n, n = q, q = m & \text{any two indices repeated} \end{cases}$$



Atmospheric Dynamics: Mechanical Energy Equation

Mechanical Energy Equation

- The mechanical energy equation describes the rate of change of a fluid element's kinetic energy.
- To start, we take the dot product of the velocity vector with our momentum balance equation.

$$\vec{U} \cdot \left(\underbrace{\rho \frac{D\vec{U}}{Dt}}_1 = \underbrace{-\vec{\nabla} p}_2 - \underbrace{2\rho\vec{\Omega} \times \vec{U}}_3 + \underbrace{\rho\vec{g}}_4 + \underbrace{\mu\vec{\nabla}^2\vec{U}}_5 \right)$$

- Note: We've multiplied the momentum balance equation by ρ
- We will examine each term separately and then put together for our final expression.



Mechanical Energy Equation

Term 1

$$\begin{aligned}\vec{U} \cdot \rho \frac{D\vec{U}}{Dt} &= u_i \left(\rho \frac{\partial u_i}{\partial t} + \rho u_j \frac{\partial u_i}{\partial x_j} \right) \\ &= \rho u_i \frac{\partial u_i}{\partial t} + \rho u_j u_i \frac{\partial u_i}{\partial x_j} \quad \text{use product rule} \\ &= \rho \frac{\partial \left(\frac{u_i u_i}{2} \right)}{\partial t} + \rho u_j \frac{\partial \left(\frac{u_i u_i}{2} \right)}{\partial x_j} \\ &= \boxed{\rho \frac{\partial E}{\partial t} + \rho u_j \frac{\partial E}{\partial x_j}}\end{aligned}$$

where $E = u_i^2/2$ is kinetic energy.



Term 2

$$\begin{aligned}\vec{U} \cdot (-\vec{\nabla}p) &= -u_i \frac{\partial p}{\partial x_i} \quad \text{use product rule} \\ &= -\left(\frac{\partial(pu_i)}{\partial x_i} + p \frac{\partial u_i}{\partial x_i} \right) \\ &= -\frac{\partial(pu_i)}{\partial x_i}\end{aligned}$$



Mechanical Energy Equation

Term 3

$$\vec{U} \cdot (-2\rho\vec{\Omega} \times \vec{U})$$

Recall that the Coriolis has the following components:

- x : fv
- y : $-fu$
- z : 0

This corresponds to $\epsilon_{ij3}fu_j$. So,

$$\vec{U} \cdot (-2\rho\vec{\Omega} \times \vec{U}) = \boxed{\epsilon_{ij3}fu_iu_j}$$

However, using the rules of the alternating unit tensor, you can show this is equal to zero. Alternatively, you know $-2\rho\vec{\Omega} \times \vec{U}$ is \perp to \vec{U} . Thus, their dot product is zero. Why?

Coriolis force does no work!



Term 4

$$\vec{U} \cdot \vec{g} = u_i g_i$$

But if we assume that gravity only acts in the \hat{k} direction, then we can make use of the Kronecker delta:

$$\vec{U} \cdot \rho \vec{g} = \boxed{\rho u_i g_i \delta_{i3}}$$



Term 5

$$\begin{aligned}\vec{U} \cdot \nu \vec{\nabla}^2 \vec{U} &= \mu u_i \frac{\partial^2 u_i}{\partial x_j^2} \\ &= \mu u_i \frac{\partial}{\partial x_j} \frac{\partial u_i}{\partial x_j} \\ &= \boxed{u_i \frac{\partial \tau_{ij}}{\partial x_j}}\end{aligned}$$



All Together

$$\underbrace{\rho \frac{\partial E}{\partial t}}_1 + \underbrace{\rho u_j \frac{\partial E}{\partial x_j}}_2 = - \underbrace{\frac{\partial (p u_i)}{\partial x_i}}_3 + \underbrace{\rho u_i g_i \delta_{i3}}_4 + \underbrace{u_i \frac{\partial \tau_{ij}}{\partial x_j}}_5$$

Terms

- 1 Storage of kinetic energy
- 2 Advection of kinetic energy by the bulk flow
- 3 Work done against gravity
- 4 Work done against viscous forces



Mechanical Energy Equation

- Note: we can expand the viscous dissipation term as:

$$\begin{aligned}u_i \frac{\partial \tau_{ij}}{\partial x_j} &= \frac{\partial u_i \tau_{ij}}{\partial x_j} - \tau_{ij} \frac{\partial u_i}{\partial x_j} \\ &= \frac{\partial u_i \tau_{ij}}{\partial x_j} - \tau_{ij} S_{ij}\end{aligned}$$

where S_{ij} is the symmetric part of the velocity gradient.

- The first term is the total rate of work, or molecular diffusion.
- The second term is the deformation work, or viscous dissipation.



Atmospheric Dynamics: Thermal Energy Equation

Thermal Energy Equation

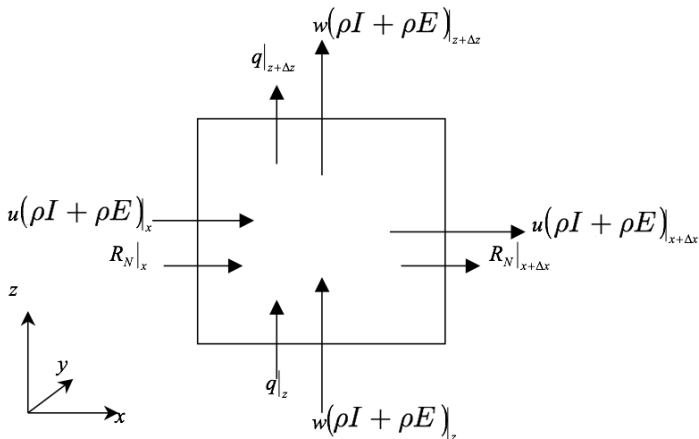
- We can write the 1st Law of Thermodynamics for an open unsteady system in words as follows, where total energy = internal (I) + kinetic ($E = V^2/2$):

$$\underbrace{\left\{ \begin{array}{c} \text{rate of} \\ \text{total energy} \\ \text{accumulation} \end{array} \right\}}_1 = \underbrace{\left\{ \begin{array}{c} \text{net rate of} \\ \text{total energy in} \\ \text{by advection} \end{array} \right\}}_2 + \underbrace{\left\{ \begin{array}{c} \text{net rate of} \\ \text{heat added by} \\ \text{conduction} \end{array} \right\}}_3 \\ + \underbrace{\left\{ \begin{array}{c} \text{net rate of} \\ \text{heat added by} \\ \text{radiation} \end{array} \right\}}_4 + \underbrace{\left\{ \begin{array}{c} \text{net rate of} \\ \text{heat added by} \\ \text{phase change} \end{array} \right\}}_5 \\ - \underbrace{\left\{ \begin{array}{c} \text{net rate of} \\ \text{work done by} \\ \text{fluid on} \\ \text{surroundings} \end{array} \right\}}_6$$



Thermal Energy Equation

- This is seen visually as:



Let's look separately at each term in the previous description.



Term 1

- Rate of accumulation of internal energy per unit volume and kinetic energy within the element (these are in units of W):

$$\Delta x \Delta y \Delta z \frac{\partial}{\partial t} (\rho I + \rho E)$$



Term 2

- Net rate of advection of internal and kinetic Energy into the volume element:

$$\begin{aligned} & \Delta y \Delta z \{u(\rho I + \rho E)_{x+\Delta x} - u(\rho I + \rho E)_x\} \\ & + \Delta x \Delta z \{v(\rho I + \rho E)_{y+\Delta y} - v(\rho I + \rho E)_y\} \\ & + \Delta x \Delta y \{w(\rho I + \rho E)_{z+\Delta z} - w(\rho I + \rho E)_z\} \end{aligned}$$



Term 3

- Net rate of energy input by conduction into the volume element (molecular):

$$\begin{aligned} \Delta y \Delta z (q_x|_x - q_x|_{x+\Delta x}) + \Delta x \Delta z (q_y|_y - q_y|_{y+\Delta y}) \\ + \Delta x \Delta y (q_z|_z - q_z|_{z+\Delta z}) \end{aligned}$$



Term 4

- Net rate of energy input by all wavelengths of radiation into the volume element:

$$\begin{aligned} \Delta y \Delta z (R_{nx}|_x - R_{nx}|_{x+\Delta x}) + \Delta x \Delta z (R_{ny}|_y - R_{ny}|_{y+\Delta y}) \\ + \Delta x \Delta y (R_{nz}|_z - R_{nz}|_{z+\Delta z}) \end{aligned}$$



Term 5

- Net rate of energy input by phase change into the volume element:

$$\Delta x \Delta y \Delta z (L_v \epsilon)$$

where L_v ($\sim 2.45 \times 10^6 \text{ J kg}^{-1}$) is the latent heat of vaporization/condensation and ϵ ($\text{kg m}^{-3} \text{ s}^{-1}$) is the evaporation/condensation rate per unit volume.

- Note: this is a body sink/source term.



Term 6

- Net rate of work done by the fluid element against the surroundings.
- Recall that work rate done by a force is the magnitude of the force multiplied by the velocity in the direction of the force:

$$\dot{W} = \vec{F} \cdot \vec{U}$$

So we will write the work rates as forces multiplied by velocities acting on our fluid element.

- The net rate of work will be broken into work against body forces and work against surface forces.



Thermal Energy Equation

Term 6

- Work against body forces: rate of doing work against the gravitational force

$$\Delta x \Delta y \Delta z (\rho u g_x + \rho v g_y + \rho w g_z)$$

- Work against surface forces: rate of doing work against the pressure at the six faces of a volume element

$$\begin{aligned} \Delta y \Delta z \{ (pu)_x|_{x+\Delta x} - (pu)_x|x \} &+ \Delta x \Delta z \{ (pv)_y|_{y+\Delta y} - (pv)_y|_y \} \\ &+ \Delta x \Delta y \{ (pw)_z|_{z+\Delta z} - (pw)_z|_z \} \end{aligned}$$

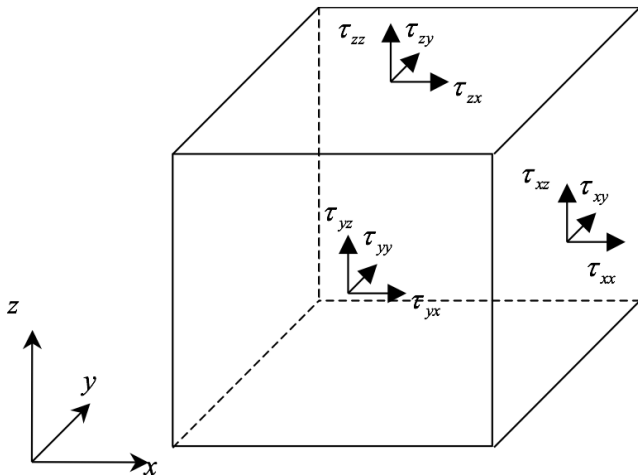
Note that here we take the work rate to be $(p \cdot \vec{n} dA) \cdot \vec{U}$ where \vec{n} is the outwardly pointing normal vector from the fluid element.



Thermal Energy Equation

Term 6

- Work against surface forces: rate of doing work against the viscous force



Term 6

- Work against surface forces: rate of doing work against the viscous force

$$\begin{aligned} & \Delta y \Delta z \{ (\tau_{xx}u + \tau_{xy}v + \tau_{xz}w)_x - (\tau_{xx}u + \tau_{xy}v + \tau_{xz}w)_{x+\Delta x} \} \\ & + \Delta x \Delta z \{ (\tau_{yx}u + \tau_{yy}v + \tau_{yz}w)_y - (\tau_{yx}u + \tau_{yy}v + \tau_{yz}w)_{y+\Delta y} \} \\ & + \Delta x \Delta y \{ (\tau_{zx}u + \tau_{zy}v + \tau_{zz}w)_z - (\tau_{zx}u + \tau_{zy}v + \tau_{zz}w)_{z+\Delta z} \} \end{aligned}$$



Thermal Energy Equation

All Together

- Now we combine all terms, divide by $\Delta x \Delta y \Delta z$, and take the limit as $\Delta x \rightarrow 0$, $\Delta y \rightarrow 0$, and $\Delta z \rightarrow 0$ to obtain the **complete energy equation**:

$$\begin{aligned} \frac{\partial(\rho I + \rho E)}{\partial t} = & - \left(u \frac{\partial(\rho I + \rho E)}{\partial x} + v \frac{\partial(\rho I + \rho E)}{\partial y} + w \frac{\partial(\rho I + \rho E)}{\partial z} \right) \\ & - \left(\frac{\partial q_x}{\partial x} + \frac{\partial q_y}{\partial y} + \frac{\partial q_z}{\partial z} \right) - \left(\frac{\partial p u}{\partial x} + \frac{\partial p v}{\partial y} + \frac{\partial p w}{\partial z} \right) \\ & - \left(\frac{\partial R_{nx}}{\partial x} + \frac{\partial R_{ny}}{\partial y} + \frac{\partial R_{nz}}{\partial z} \right) - \left(\frac{\partial u g_x}{\partial x} + \frac{\partial v g_y}{\partial y} + \frac{\partial w g_z}{\partial z} \right) \\ & - L_v \epsilon \\ & - \left\{ \frac{\partial(\tau_{xx} u + \tau_{yx} v + \tau_{zx} w)}{\partial x} + \frac{\partial(\tau_{xy} u + \tau_{yy} v + \tau_{zy} w)}{\partial y} \right. \\ & \left. + \frac{\partial(\tau_{xz} u + \tau_{yz} v + \tau_{zz} w)}{\partial z} \right\} \end{aligned}$$



Thermal Energy Equation

All Together

- As with the derivation of the momentum equation, we can utilize Newtonian expressions to relate the velocity gradients and stresses, namely:

$$\begin{aligned}\tau_{xx} &= -2\mu \frac{\partial u}{\partial x} + \frac{2}{3}\mu(\vec{\nabla} \cdot \vec{U}) & \tau_{xy} &= \tau_{yx} = -\mu \left(\frac{\partial u}{\partial y} + \frac{\partial v}{\partial x} \right) \\ \tau_{yy} &= -2\mu \frac{\partial v}{\partial y} + \frac{2}{3}\mu(\vec{\nabla} \cdot \vec{U}) & \tau_{xz} &= \tau_{zx} = -\mu \left(\frac{\partial u}{\partial z} + \frac{\partial w}{\partial x} \right) \\ \tau_{zz} &= -2\mu \frac{\partial w}{\partial z} + \frac{2}{3}\mu(\vec{\nabla} \cdot \vec{U}) & \tau_{zy} &= \tau_{yz} = -\mu \left(\frac{\partial w}{\partial y} + \frac{\partial v}{\partial z} \right)\end{aligned}$$

Or more compactly:

$$\tau_{ij} = -2\mu S_{ij} + \frac{2}{3}\mu(\vec{\nabla} \cdot \vec{U})\delta_{ij}$$



Thermal Energy Equation

All Together

- We now subtract the E equation (slide 13) from the complete energy equation to yield the **thermal energy equation**:

$$\underbrace{\rho \frac{DI}{Dt}}_1 = - \underbrace{\vec{\nabla} \cdot \vec{q}}_2 - \underbrace{\vec{\nabla} \cdot (p\vec{U})}_3 - \underbrace{\vec{\nabla} \cdot \vec{R}_n}_4 + \underbrace{L_v \epsilon}_5 + \underbrace{\mu \Phi_\nu}_6$$

Terms (per unit volume)

- 1 Rate of gain of internal energy
- 2 Rate of internal energy input by conduction
- 3 Reversible rate of internal energy increase by compression
- 4 Rate of internal energy input by net radiation
- 5 Rate of internal energy input by phase change
- 6 Irreversible rate of internal energy increase by viscous dissipation



Thermal Energy Equation

- The viscous term written out in full is:

$$\Phi_\nu = -2\mu S_{ij}S_{ij} + \frac{2}{3}\mu(\vec{\nabla} \cdot \vec{U})^2$$

- The thermal energy equation is written in terms of internal energy.
- However, we want to express the equation in terms of temperature and heat capacity.
- Let's work to relate I to T , θ and c_p , c_v .



Thermal Energy Equation

- Recall from thermodynamics that $I = I(\alpha, T)$, where α is the specific volume and T the absolute temperature.
- Thus,

$$dI = \left(\frac{\partial I}{\partial \alpha} \right)_T d\alpha + \left(\frac{\partial I}{\partial T} \right)_\alpha dT$$

- Multiplying by the density and considering the substantial derivatives:

$$\rho \frac{DI}{Dt} = \left(\frac{\partial I}{\partial \alpha} \right)_T \rho \frac{D\alpha}{Dt} + \rho c_v \frac{DT}{Dt}$$

where c_v is the specific heat of the fluid at constant volume.



Thermal Energy Equation

- Writing the specific volume as the inverse of the density and using the product rule of calculus:

$$\rho \frac{D\alpha}{Dt} = \rho \frac{D}{Dt} \left(\frac{1}{\rho} \right) = -\frac{1}{\rho} \frac{D\rho}{Dt} = -\frac{1}{\rho} \vec{\nabla} \cdot \vec{U}$$

- Then for incompressible flow where $\vec{\nabla} \cdot \vec{U} = 0$ we have:

$$\rho c_v \frac{DT}{Dt} = -\vec{\nabla} \cdot \vec{q} - \vec{\nabla} \cdot \vec{R}_n + L_v \epsilon + \mu \Phi'_\nu$$

where the viscous dissipation term simplifies to:

$$\Phi_\nu = -2\mu S_{ij} S_{ij}$$



Thermal Energy Equation

- Using Fourier's Law of Heat Conduction allows us to write the second term as a function of temperature:

$$\vec{q} = -\kappa \vec{\nabla} T$$

where κ is the thermal conductivity of the fluid. Thus,

$$-\vec{\nabla} \cdot \vec{q} = \kappa \vec{\nabla} \cdot \vec{\nabla} T = \kappa \vec{\nabla}^2 T$$

- Substitution yields the thermal energy equation in terms of T :

$$\rho c_v \frac{DT}{Dt} = \kappa \vec{\nabla}^2 T - \vec{\nabla} \cdot \vec{R}_n + L_v \epsilon + \mu \Phi'_\nu$$

This equation yields temperature changes from heat conduction, radiation divergence, phase change, and viscous heating



Thermal Energy Equation

- For a constant pressure fluid we can make the following substitution:

$$dI = -pd\alpha + c_p dT$$

which for an incompressible fluid leads to

$$\rho c_p \frac{DT}{Dt} = \kappa \vec{\nabla}^2 T - \vec{\nabla} \cdot \vec{R}_n + L_v \epsilon + \mu \Phi'_\nu$$

which is essentially stating that we can switch between c_v and c_p , which is justified when the pressure terms are neglected in a gas flow energy equation.



Thermal Energy Equation

- The expression is approximately an enthalpy change:

$$\frac{DT}{Dt} = \frac{\kappa}{\rho c_p} \vec{\nabla}^2 T - \frac{1}{\rho c_p} \vec{\nabla} \cdot \vec{R}_n + \frac{L_v \epsilon}{\rho c_p} + \frac{\mu \Phi'_\nu}{\rho c_p}$$

- If viscous heating is small and we define thermal diffusivity as $K = \kappa/c_p T$:

$$\frac{DT}{Dt} = K \vec{\nabla}^2 T - \frac{1}{\rho c_p} \vec{\nabla} \cdot \vec{R}_n + \frac{L_v \epsilon}{\rho c_p}$$

or for potential temperature:

$$\frac{D\theta}{Dt} = K \vec{\nabla}^2 \theta - \frac{1}{\rho c_p} \vec{\nabla} \cdot \vec{R}_n + \frac{L_v \epsilon}{\rho c_p}$$



We have now derived the following basic equations of atmospheric dynamics, assumptions, approximations, and specific cases of their application:

- Conservation of momentum
- Assumptions and approximations to the momentum equation
- Ekman layer
- Taylor-Proudman Theorem
- Thermal wind
- Mechanical energy equation
- Thermal energy equation

